

Evaluation of Solid Sorbents as a Retrofit Technology for CO₂ Capture



DE-FE0004343

Project Update: July 10, 2012



Presentation Outline

- Background
 - Participants
 - Project Goals
 - Project Overview
- 1 MW Pilot
 - Sorbent Characteristics
 - Contactor Design Selection
 - Host Site Information
 - Project Accomplishments
 - Future Plans

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ADA CO₂ Capture Program

• Phase I – Viability Assessment

- Cooperative Agreement: DE-NT0005649
 - Dual Focus: Sorbents & Process
 - 1 kW_e Test Device

• Phase II – FEED & Pilot Testing

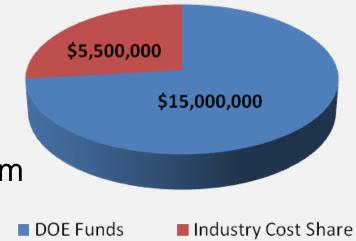
- Cooperative Agreement: DE-FE0004343
 - Sorbent Selection & Reactor Design
 - Full-Scale Conceptual Design
 - 1 MW_e Pilot Unit
 - Techno-Economic Assessment
- Phase III (Demonstration)
 - Full-Scale Preliminary Design
 - Validate Design (>25 MW_e)





Project Goals

- The overall objective of this funding stage is to validate solid sorbent-based post combustion CO₂ capture through slipstream pilot testing.
- Project Goals:
 - Achieve 90% CO₂ Capture
 - LCOE increase less than <35%
 - o Generate a high purity CO₂ stream
 - Successfully scale sorbents



Federal Funding provided by the DOE National Energy Technology Laboratory's Innovations for Existing Plants Program

Project Objectives

- Reduction in energy penalty and costs associated with post-combustion CO₂ capture
- Reduction in overall environmental impacts versus other CO₂ capture options
- Reliable operation
- Applicable to retrofit and new builds
- Period of Performance:
 - October 1, 2010 December 31, 2014

Project Participants

• DOE – NETL

• Project Sponsor

• ADA-ES, Inc.



- Project Management
- Sorbent Evaluation & Selection
- Conceptual Process Design
- Techno-Economic Assessment
- Shaw Energy & Chemicals, Inc.
 - Detailed Engineering Services
 - Significant Experience with
 Fluidized Bed Reactor Design
 - Isothermal and Adiabatic Reactors
 - Single & Multibed Reactors

- Stantec Consulting Ltd.
 - o Cost Analysis
 - o Plant Integration



- Owners Engineer
 Perspective
- EPRI



- ELECTRIC POWER RESEARCH INSTITUTE
- Industry Cost Share
- Independent Performance
 Evaluation and Techno Economic Assessment
- Southern Company
 - o Host Site
 - o Cost Share

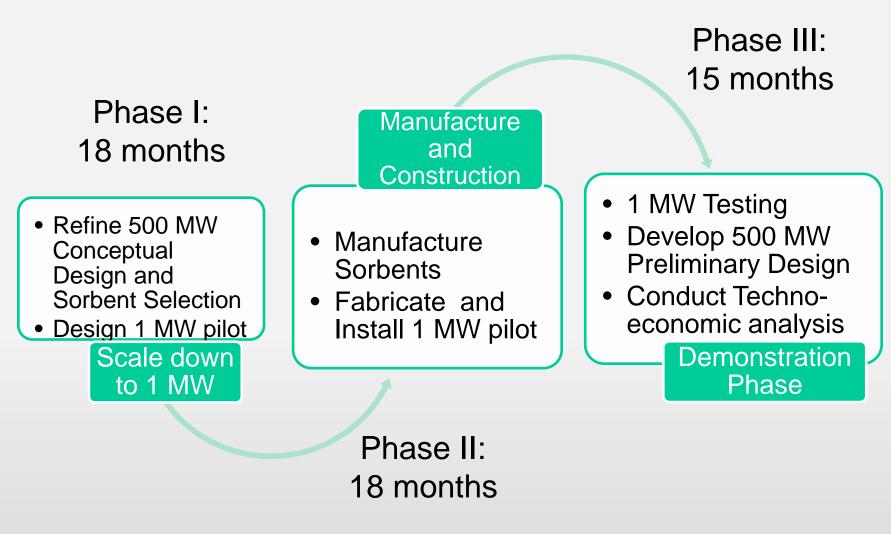


Luminant

 Cost Share

Luminant

Project Budget Period Overview



Potential Benefits of Solid Sorbents

- Energy Penalty
 - Sensible heat requirement is less although heat recovery should be considered
 - Latent heat of evaporation
- Corrosion
 - Less expensive materials of construction
 - No corrosion inhibitors required
- Air
 - Reduced emissions of amines
- Water
 - o Less cooling water required
 - o Minimal liquid waste
- Process Flexibility and Operability
 - o Can be applied to cycling plant "load following"
 - No risk of foaming or other solvent-related challenges



Sorbent Properties









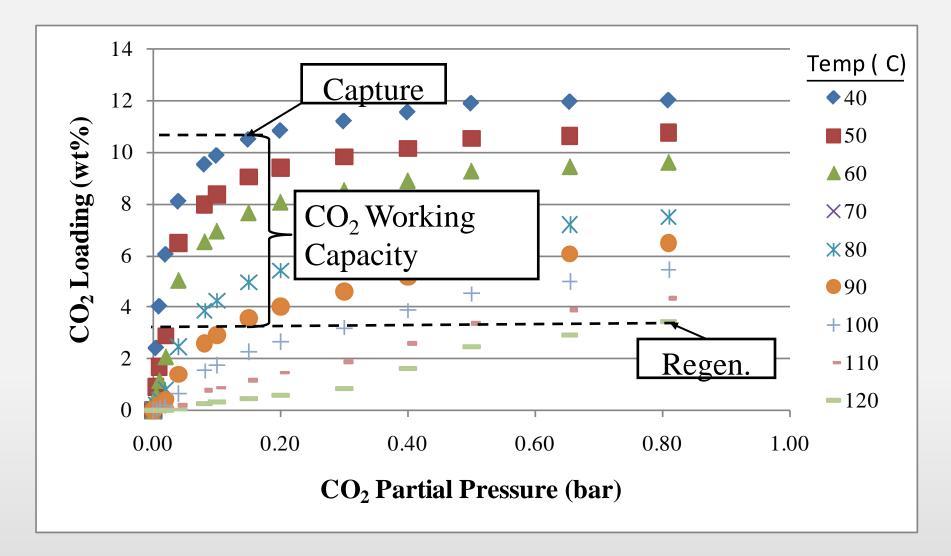
Sorbent Selection

Selection Criteria

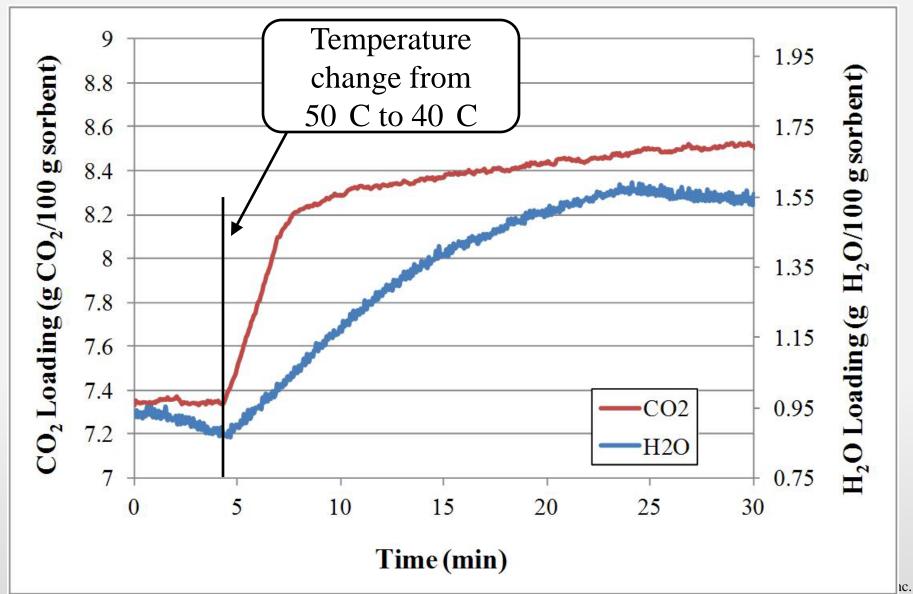
- o Kinetics
- Higher working CO₂ delta loading
- o Stability
- Part of a commercial process
- Experience with changing particle size
- Potential regeneration after the formation of heat stable salts
- 1MW Pilot Capacity
 - Approximately 5 tons (dry basis) required for operation
 - o Batches will have same specifications
 - QC checks through lab scale testing



Sorbent Isotherms



Sorbent Kinetics





1 MW Pilot Design









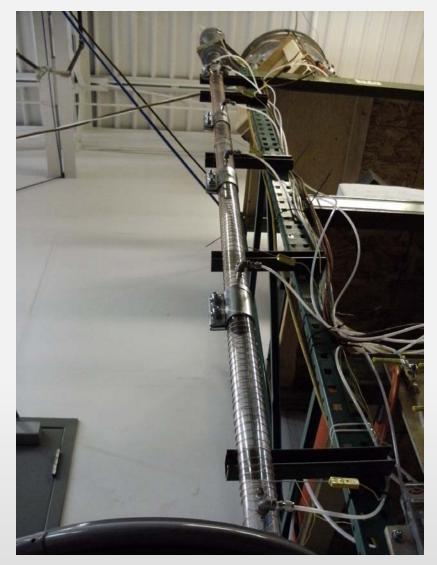
Design Considerations

- Capital costs
- Gas/solids contacting
- Heat transfer
- Sorbent attrition
- Pressure drop
- Maintenance requirements
- Footprint

Designs Considered

Comparison

- Similar
 - Capital costs
 - o Footprint
- Advantage TDR
 - Pressure drop
 - o Attrition
- Advantage SFB
 - o Gas/solids contacting
 - Heat transfer
 - o Commercial design

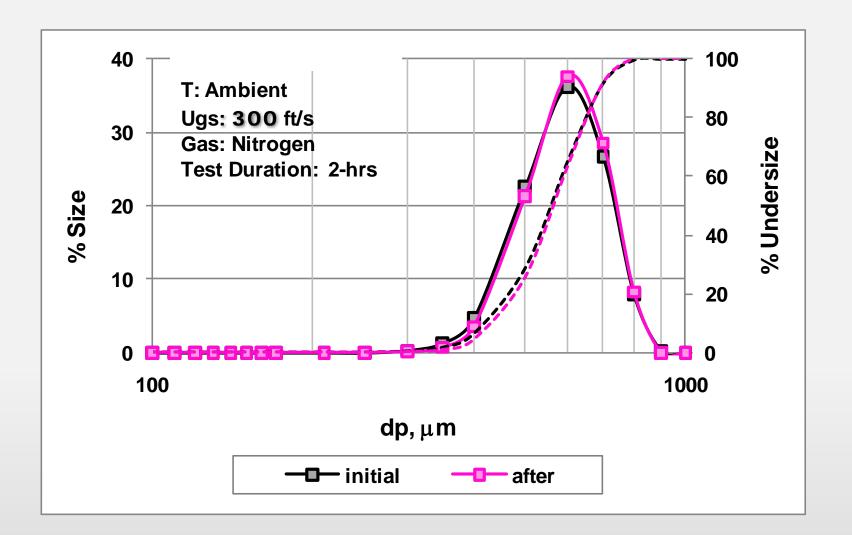


Fluidization Characterization

- Variables
 - o Sorbent particle size
 - o Gas velocity: (1-5 ft/s)
- Measurements
 - o Fluidization regime
 - Pressure drop (average and fluctuations)
 - Heat transfer coefficient
 - o Entrainment rate
- Results
 - o Optimized particle size distribution
 - o Bed density: 15-30 lb/ft³
 - o Heat transfer coefficient: 65-105 Btu/hr·ft² F
 - o Entrainment flux: provided operation limits



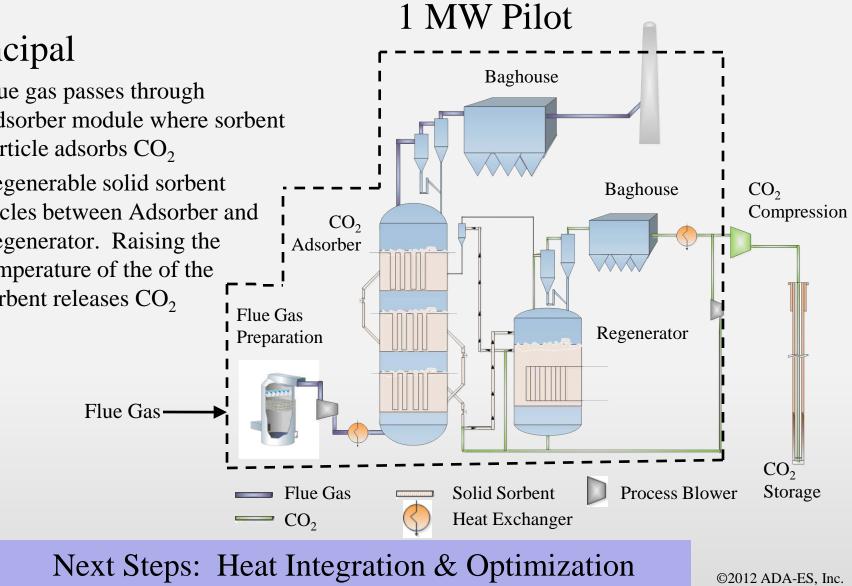
Mechanical Attrition Test Results



Process Conceptual Design

Principal

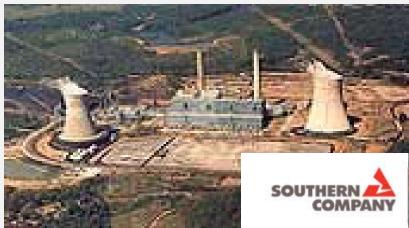
- Flue gas passes through ۲ Adsorber module where sorbent particle adsorbs CO₂
- Regenerable solid sorbent ٠ cycles between Adsorber and CO Regenerator. Raising the Adsorber temperature of the of the sorbent releases CO_2

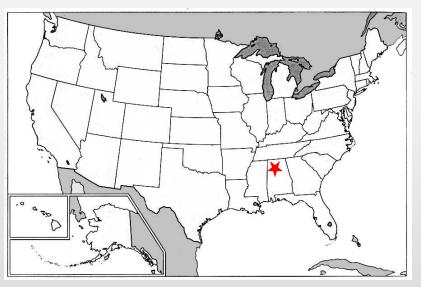


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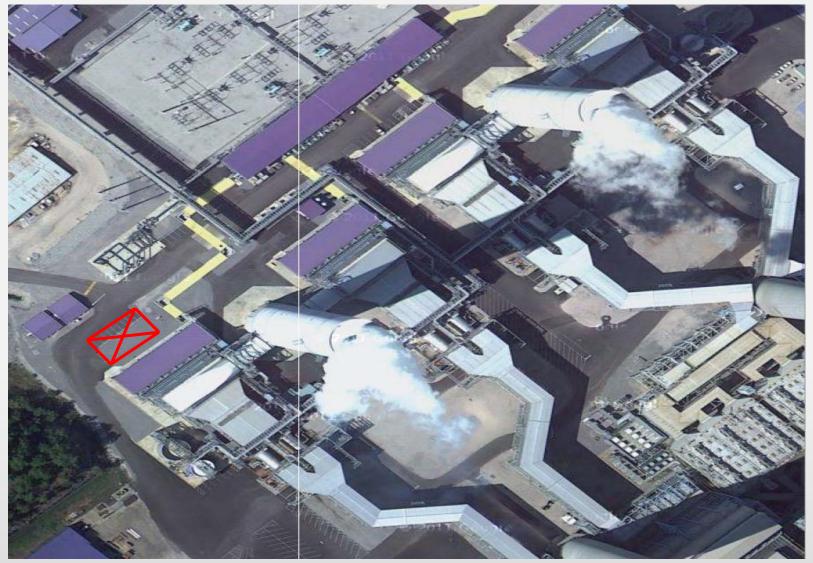
Host Site

- Host Site: Southern Company Alabama Power Co. Plant Miller
 - \circ 4 EGUs (~2,640 MW_e)
 - o Flagship Plant
 - o PRB Coal
 - o WFGD
 - Pilot Located near WFGD on Unit 1





1 MW Pilot Location



1 MW Pilot Project Schedule

Milestone Description	Date
Start site work for 1 MW pilot	4Q12
Substantial completion of mechanical installation SOW	3Q13
Substantial completion of electrical SOW	4Q13
Demonstrate pilot operation	1Q14
Begin continuous performance testing	1Q14
Complete field testing	2Q14



Budget Period 2 Scope

- Procure and Manufacture Sorbents
- Procure and Fabricate Pilot-Scale Equipment
 - Procure Pilot Scale Equipment
 - Finalize Fabrication and Construction Work Packages
 - Equipment and Module Fabrication

Installation and Startup

- o Host-site Preparation
- o Mechanical Installation
- o Electrical Installation
- Commissioning/Startup Activities

Budget Period 3 Scope

- Pilot Scale Operation and Evaluation
 - Parametric Testing

60 Day Continuous Performance Test

- Define and Collect Compression and Sequestration Information
- Prepare Commercial Design Specifications

 Refine Full-Scale Design Specifications
 Full-Scale Conceptual Engineering Design
 Conduct Full-Scale System Economic Evaluation
 Heat Recovery Information



Creating a Future with Cleaner Coal

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